Date of Survey	Tank Number	Tank Design	Contents of Tank	Material Composition (% Volume)	Vapor Pressure (psi)	Temperature in F	Tank Movement	Tank Maintenance
1/13/2010	A330	External Floating Roof Double Seal	Maya Crude	n-butane 0.36 isopentane 0.65 n-pentane 0.83 cyclopentane 0.08 n-hexane 0.70 methylcyclopentane 0.34 benzene 0.03 cyclohexane 0.23 C ₆ isoparaffins 0.78 Total Sulfur 3.76	3	95.9	Static, 51 feet, 1 ½ inches	None
1/13/2010	A332	External Floating Roof Double Seal	Maya Crude	See A330	3	85	Empty, 7 feet	None
1/13/2010	A333	External Floating Roof Double Seal	Maya Crude	See A330	3	89.9	Static, 51 feet, 2 ³ ⁄ ₄ inches	None
1/14/2010	A310	External Floating Roof Double Seal	Bonga Crude	Crude Oil 100% Hydrogen Sulfide, Variable Natural Gas Variable Benzene Variable N-Hexane Variable	4	64	Static, 7 feet 7 inches	None
1/14/2010	A318	Walls cut out to facilitate maintenance activity	HAD DU2 Rerun Slop Oil	Composition in % weight Crude Oil Sour 100% weight n-Hexane (from crude) Variable Benzene (from crude) Variable Natural Gas (from crude) Variable Sulfur > 0.5%	0.01 PSI	Ambient	Maintenance activities	Cleaning out tank, Frac tanks used to store tank waste
1/14/2010	A319	External Floating Roof Double Seal	Rerun Slop Oil	Composition in % weight Crude Oil Sour 100% weight n-Hexane (from crude) Variable Benzene (from crude) Variable Natural Gas (from crude) Variable Sulfur > 0.5%	0.8	Ambient	Out of service, 4 feet of product in tank	None
1/14/2010	G324	External Floating Roof Double Seal	Bonga Crude	Composition in % weight Crude Oil Sour 100% weight n-Hexane (from crude) Variable	2.6 PSI	50.8	Static, 7 feet 9 inches	None

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Date of Survey	Tank Number	Tank Design	Contents of Tank	Material Composition (% Volume)	Vapor Pressure (psi)	Temperature in F	Tank Movement	Tank Maintenance
				Benzene (from crude) Variable Natural Gas (from crude) Variable Sulfur > 0.5%				
1/15/2010	AP16	Cone Internal Floating Roof	Cat Crack Feed	P High Sulfur, Catalytic Cracker Feed Mixture 100% 1 Heavy Gas Oil 0-100% 2 Vacuum Gas Oil 0-100% 3 Coker Gas Oil 0-100% 4 Hydrogen Sulfide <0.04%	0.008	83	Static 35 feet 35 inches	?
1/15/2010	AP17	Cone Internal Floating Roof	Cat Crack Feed	P High Sulfur, Catalytic Cracker Feed Mixture 100% 1 Heavy Gas Oil 0-100% 2 Vacuum Gas Oil 0-100% 3 Coker Gas Oil 0-100% 4 Hydrogen Sulfide <0.04%	0.008	55	Static2 feet 6 inches	?
1/15/2010	AP18	Internal Floating Roof	Py Gas	Composition in % Light Catalytic Cracked Petroleum Naptha 0 –100% Heavy Catalytic Cracked Petroleum Naptha 0 –100% Gasoline, Pyrolysis 0 –100% Debutanizer Bottoms 0 –100% Xylene 0-15% Toluene 0-10% 1,2,4-Trimethylbenzene 0-7%	2	41	Static 7 foot 8 3⁄4 inches	Olefins 6-7008
1/15/2010	AP19	External Floating Roof	Gasoline (Naphtha)		500 –700 mm HG at 21degrees C	41	Static 7 foot 6 inches, out of service	Olefins 6-7008
1/23/2010 wind direction out of SE	J327	Vertical Fixed Roof Tank	Distilling Kerosene	Percent Total Liquid Weight Kerosene 100	0.03 psia	96	Static, 20 feet	None
1/23/2010 wind direction out of SE	J328	Vertical Fixed Roof Tank	Distilling Kerosene	Percent Total Liquid Weight Kerosene 100	0.03 psia	96	Static 21 Feet	JOSEPH
1/23/2010	J329	Internal						Tank is

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Date of Survey	Tank Number	Tank Design	Contents of Tank	Material Composition (% Volume)	Vapor Pressure (psi)	Temperature in F	Tank Movement	Tank Maintenance
wind direction out of SE		Floating Roof Tank						empty, man ways removed Out of service on 8/2005
1/23/2010 wind direction out of SE	J330	Internal Floating Roof Tank						Tank is empty, man ways removed Out of service on 8/2005
1/23/2010 wind direction out of SE	J331	Vertical Fixed Roof Tank	Hydrocrack er Feed or Heavy Gas Oil	Percent Total Liquid Weight MSDS 830348 Untreated Heavy Gas Oil 100 Haevy Gas Oil Hydrogen Sulfide <0.04	0.01 psia	68	Filling 19 feet	?
1/23/2010 wind direction out of SE	J332	Vertical Fixed Roof Tank	Hydrocrack er Feed or Heavy Gas Oil	Percent Total Liquid Weight MSDS 830348 Untreated Heavy Gas Oil 100 Haevy Gas Oil Hydrogen Sulfide <0.04	0.01 psia	68	Filling 19 feet	2
1/15/2010	A325	External Floating Roof	Maya Crude	See A330	3	50	Static 8 feet 4 inches	None
1/15/2010	A326	External Floating Roof	Maya Crude	See A330	3	56	Static 18 feet	None
2/8/2010	AP19	External Floating Roof Tank	Naphtha	N-Pentane 18.3 % N-Hexane 40.3 % N-Heptane 22 % 1-Pentene 0.2 % Cyclopentene 5.1% Benzene 4.4% Naphthlene 9.7%	1.044	55	Static 7.55 feet	none
2/8/2010	TOL91	Internal Floating Roof Tank, primary seal - mechanical	Pyrolysis Gas (PYE Gas)	Wt % 3-METHYL-1-BUTENE 0.33% ISOPENTANE 3.10% 1,4 PENTADIENE 0.33% 1-PENTENE 1.14%	10 psia	55 degrees F	Movement Filling on 2/8/2010 25 feet 8 inches at 1 PM to 26	None

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Date of Survey	Tank Number	Tank Design	Contents of Tank	Material Composition (% Volum	ne)	Vapor Pressure (psi)	Temperature in F	Tank Movement	Tank Maintenance
		shoe, no secondary seal		2-METHYL-1-BUTENE 1.12% PENTANE 1.47% ISOPRENE 2.54% TRANS-2-PENTENE 0.88% CIS-2-PENTENE 0.49% 2-METHYL-2-BUTENE 0.67% TRANS 1,3 PENTADIENE 1.43% CYCLOPENTADIENE 1.42% C5'S-IP, CPD 13.09% CIS 1,3 PENTADIENE 0.85% CYCLOPENTENE 0.97% CYCLOPENTENE 0.97% CYCLOPENTANE 0.26% BENZENE 23.63% TOLUENE 10.47% DICYCLOPENTADIENE 1.57% C11'S PLUS 8.68% C7'S THRU C10'S+ 41.24% TOTAL C4'S & LIGHTER 0.73%				feet 27 inches at 5 PM	
3/23/2010	TOL91 3	Internal Floating Roof Tank, primary seal - mechanical shoe, no secondary seal	Pyrolysis Gas (PYE Gas)	%Liquid Weight Ethylbenzene Styrene p-Xylene 2-Methylpentane m-Xylene Toluene n-Pentane 1-Pentene n-Hexane Cyclohexane Cyclopentene n-Heptane Piperylene 1,3-Cyclopentadiene 2-Methyl-1-Butene	0.0008 0.0008 0.0008 0.0008 0.0158 0.0008 0.071 0.0742 0.0148 0.0396 0.0158 0.0089 0.0403 0.0744 0.0728 0.0327	10	78	Emptying, Tank level dropped by 3.07 feet for 9 hours,	?

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Date of Survey	Tank Number	Tank Design	Contents of Tank	Material Composition (% Volu	ime)	Vapor Pressure (psi)	Temperature in F	Tank Movement	Tank Maintenance
				Isobutane	0.0075				
				Dicyclopentadiene	0.0008				
				Isopentane	0.0594				
				Isoprene	0.105				
				o-Xylene	0.0008				
3/23/2010	TOL92	Internal	Recovery	% Liquid Weight	•	1.5	63	Emptying,	?
	0	Floating Roof	Oil	C11 -C13 Hydrocarbons	42%			Tank level	_
				Benzene	15%			dropped by 0.13 feet 9	
				Toluene	13%			hours	
				Xylene, Mixed Isomers	6%				
				1,3,5-Trimethyl benzene	5.5%				
				Styrene	3.5%				
				n-Hexane	2.5%				
				2-Methylpentane	2.5%				
				Ethylbenzene	2%				
				1,3-Pentadiene	2%				
				Octane	1%				
				Butane	1%				
				Isoprene	1%				
				Pentane, iso-	1%				
				Other C5 Hydrocarbons	1%				
				2,3-Dimethyl Pentane	1%				
2/15/2010	D381	Internal Floating Roof	Off Spec Benzene	Benzene?		2.43	86	Static until 1147 at Filling at a rate of 1.09 feet per hour from 1147 to 1700	None
3/22/2010	D352	Internal	B Column	% Liquid Weight		4.8	140	Tank level	?
		Floating Roof	Tops	2,3-Dimethypentane	1		decreased by 0.08 feet in 9		
				2,4-Dimethylpentane	1			hours	
				3,3-Dimethylpentane	1				
				n-Octane	1				

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Date of Survey	Tank Number	Tank Design	Contents of Tank	Material Composition (% Volume)		Vapor Pressure (psi)	Temperature in F	Tank Movement	Tank Maintenance
				2-Methylheptane	1				
				3-Methylheptane	1				
				Methylcyclopentane	1				
				Benzene	16				
				Toluene	27				
				o-Xylene	5				
				m-Xylene	9				
				p-Xylene	4				
				Ethylbenzene	3				
				m-Ethyltoluene	1				
				1,2,4-Trimethylbenzene	2				
				1-Methyl,4 Propylbenzene	2				

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